



(11) Publication numb r: **0 321 004 B1**

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication of patent specification :
22.01.92 Bulletin 92/04

(51) Int. Cl.⁵ : **A23L 1/105, A23L 1/015**

(21) Application number : **88202394.8**

(22) Date of filing : **28.10.88**

(54) **A process for steeping cereals with a new enzyme preparation.**

The file contains technical information submitted after the application was filed and not included in this specification

(30) Priority : **17.11.87 NL 8702735**

(43) Date of publication of application :
21.06.89 Bulletin 89/25

(45) Publication of the grant of the patent :
22.01.92 Bulletin 92/04

(84) Designated Contracting States :
AT BE DE ES FR GB IT NL SE

(56) References cited :
EP-A- 0 156 174
EP-A- 0 267 637
US-A- 2 515 157
US-A- 2 555 235
US-A- 2 712 516
US-A- 3 966 971
JOURNAL OF INDUSTRIAL MICROBIOLOGY,
 vol. 2, no. 3, October 1987, pages 195-200,
 Society for Industrial Microbiology, Amster-
 dam, NL; Y.W. HAN et al.: "Phytase produc-
 tion by *Aspergillus ficuum* on semisolid
 substrate"

(56) References cited :
CHEMICAL ABSTRACTS, vol. 68, no. 11, 11th
 March 1968, page 4666, abstract no. 48355a,
 Columbus, Ohio, US; H. MLODECKI et al.:
 "Influence of culinary processes on content of
 phytin compounds in some groats and
 flakes", & **ROCZ PANSTW. ZAKL. HIG.** 18(5).
 605-610(1967)
JOURNAL OF FOOD SCIENCE, vol. 48, 1983,
 pages 953,954,985, Chicago, US; Y. LOPEZ et
 al.: "Release of phosphorus from phytate by
 natural lactic acid fermentation"

(73) Proprietor : **DORR-OLIVER INCORPORATED**
 Corporate Headquarters 77, Havemeyer Lane
 P.O. Box 9312
 Stamford Connecticut 06904-9312 (US)
 Proprietor : **Alko Ltd.**
 P.O. Box 350
 SF-00101 Helsinki (FI)

(72) Inventor : **Vaara, Timo**
 Itainen Puistotie 16
 SF-00140 Helsinki (FI)
 Inventor : **Vaara, Martti**
 Aino Ackentie 10A
 SF-00400 Helsinki (FI)
 Inventor : **Simell, Maarit**
 Emmannankuja 1D
 SF-01670 Vantaa (FI)
 Inventor : **Lehmussaari, Antti**
 Tiovojentie 6
 SF-05200 Rajamäki (FI)
 Inventor : **Caransa, Abraham**
 56 Langs De Baan
 NL-1422 KZ Uithoorn (NL)

(74) Representative : **Kooy, Laendert Willem et al**
OCTROOIBUREAU VRIESENDORP & GAADE
 P.O. Box 266
 NL-2501 AW The Hague (NL)

EP 0 321 004 B1

Note : Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid (Art. 99(1) European patent convention).

Description

The invention relates to a process for steeping corn or sorghum kernels in warm water containing sulfur dioxide. Hereinafter for convenience we will only mention corn. Steeping of corn kernels is the first step in the processing of corn to obtain different product fractions like germs, proteins and starch. In this first step the hard corn kernels are steeped to soften them. The kernels absorb water and they swell. At the same time water-soluble substances are leached out of the corn and pass into the steepwater. The temperature of the steepwater is mostly 40-55°C. The sulfur dioxide which in general is present for about 0.2%, breaks the cell wall structure and prevents the growth of microorganisms during steeping. The steeping process lasts about 48 hours. All subsequent steps, in which the different product fractions are obtained, are much shorter. The corn steep liquor (CSL) obtained is concentrated by evaporation. The product obtained will mainly be used as animal feed but also as a nutrient in microbial fermentations. The swollen kernels are further separated in germ, fiber, starch and protein fractions in different steps.

Just like in many other plant seeds phytic acid, the hexaphosphate ester of myoinositol, is present in the corn kernels. Phytic acid mostly appears in the form of calcium and magnesium salts, which in general are called phytin. A large part of the phosphorus present in plants is stored in these compounds. In the steeping process the largest part of the phytic acid comes in the CSL. It forms an undesirable component therein for the following reasons.

Phytic acid in CSL deposits a sludge with proteins and metal ions. This has caused problems in concentrating by evaporation, transporting and storing the CSL.

When used as a nutrient in microbial fermentations, CSL is diluted and the pH is raised to 4-5. When this medium is sterilized the phytic acid forms a precipitate coating on the inner surface of the fermentor. This precipitate is hard to scrub off afterwards and it also interferes with the purification of the fermentation end products.

When CSL is used as animal feed the phytic acid present gives the following problems. Phytic acid, because it interacts with multivalent metal ions, interferes with the assimilation of various metals in the body of animals (and humans). This may lead to deficiency disorders. Phytic acid would also inhibit various enzymes in the body such as pepsin. Besides, the phosphate present in the phytic acid is not available for monogastric animals, because they only can digest phytic acid to a restricted extent.

US patent specification 2,515,157 describes a process for the treatment of CSL to obtain an improved nutrient for antibiotic fermentations. In this process the phytic acid is removed by adding an aluminium ions furnishing compound to the CSL at low pH, heating and separating the aluminium phytate formed.

US patent specification 2,712,516 describes a similar process wherein phytate is precipitated as its calcium salt. The processes described in these US patent specifications are performed after the steeping process. Therefore, an additional step is required for removing phytic acid.

Now it has been found that this additional step can be avoided by performing the steeping in the presence of an enzyme preparation comprising one or more phytin degrading enzymes.

Accordingly this invention provides a process for steeping corn or sorghum kernels wherein said kernels are steeped in warm water containing sulfur dioxide at a temperature of from 20° to 60°C for from 12 to 48 hours in the presence of an enzyme preparation comprising at least one phytin-degrading enzyme selected from a group consisting of phytases or acid phosphatases in an amount capable of substantially degrading the phytin in said kernels.

The use of phytin degrading enzymes in the treatment of phytin containing solutions in order to reduce the phytin content of said solutions is known per se. For example, US-A-3,966,971 describes the treatment of certain processed vegetable materials with acid phytase and acid protease. The starting material is at least partially ground material, e.g. soy flakes, ground soybean, cottonseed flour, but not corn or sorghum. Also, every process described in this reference includes a preliminary treatment of the vegetable material culminating in centrifugation. The solids are then resuspended in water and treated with phytase. In contrast, the present process comprises an enzyme treatment of corn and sorghum kernels during steeping without prior complex chemical and/or physical treatment.

This invention provides in particular a process for processing corn or sorghum, which comprises the consecutive steps of

- a) steeping corn or sorghum kernels in warm water containing sulfur dioxide in the presence of an enzyme preparation comprising one or more phytin degrading enzymes,
- b) separating the steepwater from the kernels and concentrating it,
- c) milling the kernels coarsely and separating and dewatering germs,
- d) fine-milling the kernels, separating fibers from starch and protein, and dewatering the fiber fraction, and
- e) separating starch and protein from each other, concentrating the protein fraction and drying and/or converting the starch fraction.

Probably the enzyme preparation comprises such an amount of one or more phytin degrading enzymes that the phytin present in the kernels is substantially degraded. With the term "phytin" used herein the salts of phytic acid and also phytic acid itself are meant.

Phytin degrading enzymes dephosphorylate inositol phosphates to yield inositol and orthophosphate. Phytin degrading enzymes include phytase and acid phosphatases. Phytase and acid phosphatases are produced by various microorganisms like *Aspergillus* spp., *Rhizopus* spp. and yeasts (Appl. Microbiol. 16 (1968) 1348-1357; Enzyme Microb. Technol. 5 (1983), 377-382) while phytase is also produced by various plant seeds, as for example wheat, during germination. Phytin degrading enzymes are very active at the low pH of the steep-water. According to methods known in the art enzyme preparations can be obtained from the above mentioned organisms. It is found that phytin in corn is degraded most efficiently with enzymes from *Aspergillus* spp. Thus, at the same enzyme dosage an *Aspergillus niger* enzyme preparation is more efficient than wheat phytase.

Microbially produced enzyme preparations may comprise additional plant material degrading enzymes such as enzymes having cellulase, hemicellulase and/or pectinase activity. These other activities contribute to the advantages which are obtained by the process of the invention. Suitable enzyme preparations are for example enzymes of the Econase EP 43 series manufactured by Alko Ltd.

The temperature during the steeping process according to the invention is 20-60°C, and generally about 50°C. The applied amount of enzyme preparation depends on the preparation used, the phytin contents of the corn kernels and the reaction conditions. The right dosage can easily be estimated by a person skilled in the art.

The process according to the invention offers, besides avoiding an additional step, various important advantages. First, by adding the enzyme preparation the steeping process is accelerated to such an extent that the steeping time may be reduced considerably. Since the steeping process is the longest step in total corn processing, a reduction thereof is of great economical importance. Thus the steeping process may be reduced to only 12 hours without any losses in the main product fraction yields. Preferably steeping time will be 12-18 hours, however, longer steeping times up to 48 hours are possible.

Secondly, the separation processes after the steeping process according to the invention are improved and give higher yields. When steeping is performed for e.g. 16 hours in the presence of the enzyme preparation, the yield of starch is higher than in the case of the conventional steeping process.

Thirdly, steeping corn in the presence of phytin degrading enzymes leads to corn steep liquor that does not contain phytin. As a result concentration of CSL is easier and the product obtained is excellently suitable for animal feed and for microbial fermentations.

The steeping time can yet be further reduced by performing the steeping process in two steps, first steeping for 4-10 hours, followed by milling the corn kernels and then further steeping the milled corn kernels for another 3-6 hours. Preferably the second stage of this double stage steeping is carried out in water not containing sulfur dioxide.

In the examples the process of the invention is carried out on laboratory scale by standard Pelshenke and Lindemann determination. As may be expected, the results obtained when carrying out the process industrially will be similar or even better due to improved separating techniques.

40 Example I

In a number of tests 50 g of corn kernels are steeped in water of 50°C containing 0.2% sulfur dioxide, in the presence or in the absence of an amount of Econase EP 434. This enzyme preparation has as major activities phytin and cellulose degrading activities and as minor activities hemicellulase and pectinase. The steeping times of the tests vary of from 12 to 48 hours, as shown in table A.

The enzyme dosages are presented as Phytin degrading units/g of corn. One phytin degrading unit (1 PU) is the amount of enzyme which liberates 1 nmol of inorganic phosphorus from sodium phytate per minute under standard conditions (40°C, pH 5.5). The kernels after steeping are processed further to obtain the product fractions mentioned in Table B.

50

55

TABLE A

Test	1	2	3	4	5	6
steeping time (h)	48	48	24	20	16	12
dosage of Iconase EP 434 (%g corn)	-	70	135	160	200	270

TABLE B

Results of single stage steeping

Test	Yield in % of dry weight					
	1	2	3	4	5	6
dry substance in CSL	5.28	5.61	4.78	4.72	4.23	3.91
germs	7.34	7.12	7.42	7.66	9.00	7.51
fibers (starch content) ^a	9.70 (19.01)	9.21 (17.16)	9.55 (16.91)	9.52 (8.60)	9.41 (16.71)	9.70 (17.46)
starch (protein content) ^a	64.09 (0.37)	65.49 (0.37)	65.29 (0.35)	65.38 (0.43)	66.20 (0.39)	64.00 (0.44)
gluten (protein content) ^a	7.31 (46.57)	6.24 (51.43)	7.57 (47.52)	8.12 (49.21)	6.94 (57.60)	9.42 (42.76)
dry substance in supernatant	2.21	2.23	2.88	2.89	3.00	2.59
starch recovery	94.4	96.5	96.2	96.3	97.5	94.3
total dry substance recovery	95.91	95.92	97.49	98.29	98.78	97.15

^a) expressed as % of the fraction

EP 0 321 004 B1

It appears from Table B that the starch yield after 16 or 48 hours of single stage steeping in the presence of the enzyme preparation is higher than in the case of conventional steeping without enzyme preparation, and after 12 hours of steeping in the presence of the enzyme preparation the starch yield is almost as high as in the case of conventional steeping without enzyme preparation.

Example II

50 g of corn kernels are presteeped in water of 50°C containing 0.2% sulfur dioxide and Econase EP 434 providing 135 PU/g of corn for 6 hours. Following manual degermination the product is milled coarsely. Then the germs are added back to the slurry. Thereafter the second stage of the steeping is carried out in fresh water of 50°C containing Econase EP 434 providing 135 PU/g of corn for 4 hours. The suspension obtained is processed further to obtain the product fractions mentioned in Table C.

TABLE C

	<u>Yield in % of dry weight</u>
dry substance in CSL	2.19
germs	8.80
fibers (starch content)	9.64 (20.99)
starch (protein content)	65.53 (0.37)
gluten (protein content)	6.8 (56.74)
dry substance in supernatant	5.45
starch recovery	96.5
total dry substance recovery	98.41

Note: In this test it is necessary to degerminate before milling because the mill used would damage the germ. When the double stage steeping is carried out industrially a mill would be used which will not damage the germ. Degermination is not necessary then.

Example III

CSL is diluted 1 : 10 and the pH is adjusted to 5.0. Corn flour is diluted 1 : 10 with 0.2 M citrate buffer pH 5.0. Sodium azide is added at a concentration of 0.02% to inhibit microbial growth. *Aspergillus* spp. enzyme preparation containing phytin degrading activity or wheat phytase (Sigma P-1259) is added at a dosage of 7000 PU/gram of phytin (300 PU per each ml of CSL dilution and 150 PU per each 2 grams of corn flour).

Suspensions are incubated in a shaker (250 rpm) at 50°C. At fixed intervals the reaction is stopped with equal volume of 6% (w/v) H₂SO₄. Phytate is extracted to the acidic liquid for 30 min, at room temperature. Phytic acid is then precipitated from a clear supernatant with ferric chloride. Ferric ions are removed by precipitation with sodium hydroxide. Phytate is determined by HPLC using sodium phytate as a standard.

Table D shows the residual phytin content of CSL and corn flour after incubation with phytin degrading enzymes. In experiment a) incubation is carried out with Aspergillus spp. enzyme preparation, and in experiment b) incubation is carried out with wheat phytase.

TABLE D

Comparing Aspergillus spp. enzyme preparation and wheat phytase.

Substrate	Incubation time (h)	Phytin (as phytic acid)			
		exp. a)		exp. b)	
		mg/ml	%	mg/ml	%
CSL	0	3.1	100	3.4	100
	2	2.7	87	2.4	71
	4	1.4	45	1.9	56
	10	1.0	32	2.0	59
	24	0	0	1.4	41
corn flour	0	13.6	100	11.4	100
	2	9.1	67	9.1	80
	4	0	0	7.9	69
	10	0	0	6.8	60
	24	0	0	2.3	20

Table D shows that phytic acid content can be reduced considerably with both phytin degrading enzymes. At the same enzyme dosage Aspergillus spp. enzyme preparation is more efficient than wheat phytase.

Example IV

25 g of corn kernels are steeped in 50 ml water of 50°C containing 0.2% sulfur dioxide. In the control no enzyme preparation is added and in the test according to the invention an Aspergillus spp. enzyme preparation is added at a dosage of 135 PU/g corn. Steeping time is 24 hours or 48 hours.

After steeping an amount of CSL is extracted for 30 min. with an equal volume of 6% (w/v) H₂SO₄ at room temperature. Phytic acid is precipitated from a clear supernatant with ferric chloride. Ferric ions are removed by precipitation with sodium hydroxide. Phytate is determined by HPLC using sodium phytate as a standard.

Table E shows the amount of phytic acid in CSL. Experiment a) comprises conventional steeping without phytin degrading enzymes and experiment b) comprises steeping in the presence of the above enzyme preparation.

aration.

TABLE E

Phytin content of CSL

steeping time (h)	mg phytic acid / ml CSL	
	exp. a)	exp. b)
24	1.6	0
48	3.1	0

Table E shows that when corn kernels are steeped in the presence of phytin degrading enzymes CSL is free from phytin.

Example V

Econase EP 434 and a plant cell wall degrading enzyme preparation with negligible phytin degrading activity are tested in one-step and in two-step steeping.

In one-step steeping 50 g of corn kernels are steeped in water of 50°C containing 0.2% sulfur dioxide. The dosage of Econase EP 434 is 135 PU/g corn. Equal volume of the plant cell wall degrading enzyme preparation with negligible phytin degrading activity is applied. Steeping time is 20 hours. The kernels are processed further according to Pelshenke and Lindemann method.

In two-step steeping 50 g of corn kernels are pre-steeped for 6 hours in water of 50°C containing 0.2% sulfur dioxide and Econase EP 434 providing 135 PU/g corn or an equal volume of plant cell wall degrading enzyme preparation with negligible phytin degrading activity. Following manual degermination the product is milled coarsely. Then the germs are added back to the slurry. Thereafter the second stage of the steeping is carried out for 4 hours in fresh water of 50°C containing Econase EP 434 providing 135 PU/g corn or an equal volume of plant cell wall degrading enzyme preparation with negligible phytin degrading activity. The slurry is further processed according to Pelshenke and Lindemann method.

TABLE F

Starch recoveries with different enzyme preparations.

1. Econase EP 434
2. plant cell wall degrading enzyme preparation with negligible phytin degrading activity.

Steeping process	Steeping time h	enzyme	starch recovery %
One-step	20	1	97.0
	20	2	94.4
Two-step	6 + 4	1	96.5
	6 + 4	2	91.4

It appears from Table F that the starch yield is higher when the kernels are treated with an enzyme preparation containing phytin degrading activity.

Claims

1. A process for steeping corn or sorghum kernels wherein said kernels are steeped in warm water containing sulfur dioxide at a temperature of from 20° to 60°C for from 12 to 48 hours in the presence of an enzyme preparation comprising at least one phytin-degrading enzyme selected from a group consisting of phytases or acid phosphatases in an amount capable of substantially degrading the phytin in said kernels.

2. A process according to claim 1, characterized in that the enzyme preparation additionally comprises other plant material degrading enzymes.

3. A process according to claim 2, characterized in that the plant material degrading enzymes possess cellulase, hemi-cellulase and/or pectinase activity.

4. A process according to any one of claims 1-3, characterized in that the phytin degrading enzyme preparation is obtained from wheat or *Aspergillus* spp. or from other plant or microbial sources.

5. A process according to any one of claims 1-4, characterized in that the kernels are steeped from 12-18 hours.

6. A process for processing corn or sorghum, which comprises the consecutive steps of

a) steeping corn or sorghum kernels in warm water containing sulfur dioxide,

b) separating the steepwater from the kernels and concentrating it,

c) milling the kernels coarsely and separating and dewatering germs,

d) fine-milling the kernels, separating fibers from starch and protein, and dewatering the fiber fraction, and

e) separating starch and protein from each other, concentrating the protein fraction and drying and/or converting the starch fraction, characterized in that the steeping in step a) is performed according to one of claims 1-5.

7. A process according to claims 1-6, **characterized in that** the steeping is performed in two steps, first steeping for 4-10 hours followed by milling the kernels and then further steeping the milled kernels for another 3-6 hours.

8. A process according to claim 7, **characterized in that** the second stage of the steeping is carried out in water not containing sulfur dioxide.

Patentansprüche

1. Verfahren zum Einweichen von Mais- oder Sorghum-Körnern, bei dem die Körner in schwefeldioxydhaltigem warmem Wasser bei einer Temperatur von 20° bis 60°C während 12 bis 48 Stunden in Gegenwart eines Enzympräparates eingeweicht werden, das wenigstens ein Phytin abbauendes Enzym aus der Gruppe der Phytasen oder Säurephosphatasen in einer Menge, die zu einem wesentlichen Abbau des Phytins in den Körnern in der Lage ist, umfaßt.

2. Verfahren nach Anspruch 1, **dadurch gekennzeichnet**, daß das Enzympräparat außerdem andere Pflanzenmaterial abbauende Enzyme umfaßt.

3. Verfahren nach Anspruch 2, **dadurch gekennzeichnet**, daß die Pflanzenmaterial abbauenden Enzyme Cellulase-, Hemicellulase- und/oder Pektinaseaktivität besitzen.

4. Verfahren nach einem der Ansprüche 1 bis 3, **dadurch gekennzeichnet**, daß das Phytin abbauende Enzympräparat aus Weizen oder *Aspergillus* spp. oder aus anderen pflanzlichen oder mikrobiellen Quellen erhalten wird.

5. Verfahren nach einem der Ansprüche 1 bis 4, **dadurch gekennzeichnet**, daß die Körner 12 bis 18 Stunden eingeweicht werden.

6. Verfahren zur Bearbeitung von Mais oder Sorghum mit den aufeinanderfolgenden Stufen, in denen man

a) Mais- oder Sorghum-Körner in schwefeldioxydhaltigem warmem Wasser einweicht,

b) das Einweichwasser von den Körnern abtrennt und konzentriert,

c) die Körner grob mahlt und Keime abtrennt und entwässert,

d) die Körner fein mahlt, Fasern von Stärke und Protein abtrennt und die Faserfraktion entwässert und

e) Stärke und Protein voneinander trennt, die Proteinfraction konzentriert und die Stärkefraktion trocknet und/oder umwandelt, **dadurch gekennzeichnet**, daß das Einweichen in der Stufe a) nach einem der Ansprüche 1 bis 5 durchgeführt wird.

7. Verfahren nach den Ansprüchen 1 bis 6, **dadurch gekennzeichnet**, daß das Einweichen in zwei Stufen erfolgt, wobei man zunächst 4 bis 10 Stunden einweicht, dann die Körner mahlt und dann die gemahlten Körner weitere 3 bis 6 Stunden einweicht.

8. Verfahren nach Anspruch 7, **dadurch gekennzeichnet**, daß die zweite Stufe des Einweichens in Wasser durchgeführt wird, das kein Schwefeldioxyd enthält.

Revendications

1. Procédé de trempage de grains de maïs ou de sorgho, dans lequel on fait tremper les grains dans de l'eau chaude contenant du bioxyde de soufre, à une température de 20° à 60°C, pendant 12 à 48 h en présence d'une préparation d'enzyme(s) comprenant au moins une enzyme capable de dégrader de la phytine et qui est choisie dans un ensemble consistant en des phytases ou en des phosphatases acides, enzyme(s) présente(s) en une quantité capable de dégrader essentiellement la phytine de ces grains.

2. Procédé selon la revendication 1, caractérisé en ce que la préparation d'enzyme(s) comprend en outre d'autres enzymes capables de dégrader de la matière végétale.

3. Procédé selon la revendication 2, caractérisé en ce que les enzymes capables de dégrader la matière végétale possèdent une activité de cellulase, d'hémi-cellulase et/ou de pectinase.

4. Procédé selon l'une quelconque des revendications 1 à 3, caractérisé en ce que l'on obtient la préparation des enzymes capables de dégrader la phytine, à partir du blé ou de *Aspergillus* spp ou à partir d'autres sources végétales ou microbiennes.

5. Procédé selon l'une quelconque des revendications 1 à 4, caractérisé en ce qu'on fait tremper les grains durant 12 à 18 h.

6. Procédé pour traiter du maïs ou du sorgho, qui comprend les étapes consécutives consistant à ;

(a) faire tremper des grains de maïs ou de sorgho dans de l'eau chaude contenant du bioxyde de soufre ;

(b) séparer l'eau de trempage d'avec les grains et concentrer cette eau ;

(c) broyer grossièrement les grains, et séparer les germes et enlever l'eau ;

(d) moudre finement les grains, séparer les fibres de l'amidon et de la protéine, et enlever l'eau de la fraction des fibres, et

(e) séparer l'amidon et les protéines l'un de l'autre, concentrer la fraction des protéines et la sécher et/ou convertir la fraction d'amidon, procédé caractérisé en ce qu'on effectue le trempage, à l'étape (a), en opérant selon l'une des revendications 1 à 5.

7. Procédé selon les revendications 1 à 6, caractérisé en ce qu'on effectue le trempage en deux étapes, en effectuant tout d'abord un trempage durant 4 à 10 h puis en soumettant les grains à mouture et en faisant encore tremper durant 3 à 6 h supplémentaires les grains moulus.

8. Procédé selon la revendication 7, caractérisé en ce qu'on effectue la seconde étape du trempage dans de l'eau ne contenant pas de dioxyde de soufre.

15

20

25

30

35

40

45

50

55